# A Numerical Method for Studying Impulsively Generated Convection from Heated Tubes

#### Serge D'Alessio

sdalessio@uwaterloo.ca

Department of Applied Mathematics University of Waterloo Waterloo, CANADA

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# Outline



#### Introduction



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# Flow Configuration



Fluid Properties:

- $\nu$  kinematic viscosity
- $\kappa$  thermal diffusivity
- $\boldsymbol{k}$  thermal conductivity
- $\alpha$  thermal expansion coefficient

Equation of State:

$$\rho = \rho_{\infty} [1 - \alpha (T - T_{\infty})]$$

Dimensionless Parameters:

$$Gr = \frac{\alpha g \Delta T c^3}{\nu^2 Qc}$$
 where  $c = \sqrt{a^2 - b^2}$   
and  $\Delta T = \frac{Qc}{k}$ ,  $Pr = \frac{\nu}{\kappa}$ ,  $\eta, r$ 

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Unsteady free convection from a heated tube is a fundamental problem and is of interest for theoretical and practical reasons. Applications include:

- hot wire anemometry
- thermal pollution
- design of heat exchangers

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The present study differs from previous investigations in the following ways:

- extend previous results on circular cylinders ([1])
- propose a new robust numerical method designed to capture the known physical behaviour
- offer an analytical solution procedure useful for theoretical and validation purposes

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#### Coordinate System



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## Navier-Stokes & Temperature Equations

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The dimensionless unsteady equations for a viscous, incompressible fluid in terms of the streamfunction,  $\psi$ , vorticity,  $\zeta$ , and temperature,  $\phi$ , are:

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$$\frac{\partial^2 \psi}{\partial \xi^2} + \frac{\partial^2 \psi}{\partial \theta^2} = M^2 \zeta$$

$$\frac{\partial \zeta}{\partial t} = \frac{1}{M^2} \left[ \frac{\partial \psi}{\partial \theta} \frac{\partial \zeta}{\partial \xi} - \frac{\partial \psi}{\partial \xi} \frac{\partial \zeta}{\partial \theta} + \frac{1}{\sqrt{Gr}} \left( \frac{\partial^2 \zeta}{\partial \xi^2} + \frac{\partial^2 \zeta}{\partial \theta^2} \right) + A \frac{\partial \phi}{\partial \xi} - B \frac{\partial \phi}{\partial \theta} \right]$$

$$\frac{\partial \phi}{\partial t} = \frac{1}{M^2} \left[ \frac{\partial \psi}{\partial \theta} \frac{\partial \phi}{\partial \xi} - \frac{\partial \psi}{\partial \xi} \frac{\partial \phi}{\partial \theta} + \frac{1}{\sqrt{Gr} Pr} \left( \frac{\partial^2 \phi}{\partial \xi^2} + \frac{\partial^2 \phi}{\partial \theta^2} \right) \right]$$
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where functions M, A, B are related to the geometry.

# Boundary, Initial & Integral Conditions

Surface conditions include no-slip and constant heat flux:

$$\psi = \frac{\partial \psi}{\partial \xi} = 0$$
 and  $\frac{1}{M} \frac{\partial \phi}{\partial \xi} = -1$  on  $\xi = 0$ 

Far-field conditions:  $\psi$ ,  $\zeta$ ,  $\phi \rightarrow 0$  as  $\xi \rightarrow \infty$ Initial conditions:  $\psi = \zeta = \phi = 0$  at t = 0

The vorticity can be shown to satisfy global conditions:

$$\int_0^\infty \int_0^{2\pi} e^{-n\xi} M^2 \zeta \sin(n\theta) d\theta d\xi = 0 , \ n = 1, 2, \cdots$$
$$\int_0^\infty \int_0^{2\pi} e^{-n\xi} M^2 \zeta \cos(n\theta) d\theta d\xi = 0 , \ n = 0, 1, \cdots$$

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**Boundary Layer Transformation** 

Introduce boundary-layer coordinate:  $\xi = \lambda z$ ,  $\lambda = \sqrt{\frac{4t}{\sqrt{Gr}}}$ The grid expands with time as illustrated below:





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**Boundary Layer Transformation** 

The governing equations then become:

 $\frac{\partial^2 \psi}{\partial z^2} + \lambda^2 \frac{\partial^2 \psi}{\partial \theta^2} = \lambda^2 M^2 \zeta$  $\frac{1}{M^2}\frac{\partial^2 \zeta}{\partial z^2} + 2z\frac{\partial \zeta}{\partial z} = 4t\frac{\partial \zeta}{\partial t} - \frac{\lambda^2}{M^2}\frac{\partial^2 \zeta}{\partial t^2}$  $+\frac{4t}{\lambda M^2}\left(\frac{\partial \psi}{\partial z}\frac{\partial \zeta}{\partial \theta}-\frac{\partial \psi}{\partial \theta}\frac{\partial \zeta}{\partial z}\right)-\frac{4tA}{\lambda M^2}\frac{\partial \phi}{\partial z}+\frac{4tB}{M^2}\frac{\partial \phi}{\partial \theta}$  $\frac{1}{PrM^2}\frac{\partial^2 \phi}{\partial z^2} + 2z\frac{\partial \phi}{\partial z} = 4t\frac{\partial \phi}{\partial t} - \frac{\lambda^2}{PrM^2}\frac{\partial^2 \phi}{\partial \theta^2} + \frac{4t}{\lambda M^2}\left(\frac{\partial \psi}{\partial z}\frac{\partial \phi}{\partial \theta} - \frac{\partial \psi}{\partial \theta}\frac{\partial \phi}{\partial z}\right)$ Waterloo

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# Discretization

Early stages of the flow are computed using the boundary-layer coordinate *z*. Once the boundary layer thickens the flow is computed using the original coordinate  $\xi$ . For large *Gr* it is more practical to work entirely in the coordinate *z*. The computational domain bounded by  $0 \le z \le z_{\infty}$  and  $0 \le \theta \le 2\pi$  is discretized into a uniform network of  $K \times L$  grid points located at

$$z_i = ih_z \ , \ i = 0, 1, \ldots, K \ , \ h_z = rac{z_\infty}{K}$$

$$\theta_j = jh_{\theta}, \ j = 0, 1, \dots, L, \ h_{\theta} = \frac{2\pi}{L}$$

 $z_{\infty}$  denotes the outer boundary approximating infinity.



# Solution of Streamfunction

The streamfunction is expanded into a truncated Fourier series

$$\psi(z,\theta,t) = \frac{1}{2}F_0(z,t) + \sum_{n=1}^{N} [F_n(z,t)\cos(n\theta) + f_n(z,t)\sin(n\theta)]$$

The Fourier coefficients satisfy

$$\frac{\partial^2 F_n}{\partial z^2} - n^2 \lambda^2 F_n = \lambda^2 s_n(z, t) , \ n = 0, 1, \cdots$$
$$\frac{\partial^2 f_n}{\partial z^2} - n^2 \lambda^2 f_n = \lambda^2 r_n(z, t) , \ n = 1, \cdots$$

At a fixed time these equations are effectively ODEs and are integrated using marching algorithms.



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# Solution of Streamfunction

The functions  $r_n(z, t)$  and  $s_n(z, t)$  are given by

$$s_n(z,t) = \frac{1}{\pi} \int_0^{2\pi} M^2 \zeta \cos(n\theta) d\theta$$
$$r_n(z,t) = \frac{1}{\pi} \int_0^{2\pi} M^2 \zeta \sin(n\theta) d\theta$$

and satisfy the intergal conditions

$$\int_0^\infty e^{-n\lambda z} s_n(z,t) dz = 0 , \ n = 0, 1, 2, \cdots$$
$$\int_0^\infty e^{-n\lambda z} r_n(z,t) dz = 0 , \ n = 1, 2, \cdots$$

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# Solution of Vorticity & Temperature

The transport equations for  $\zeta, \phi$  can be cast in generic form

 $t\frac{\partial \chi}{\partial t} = q(z,\theta,t)$ 

This equation is solved using the Crank-Nicholson implicit procedure. The solution is advanced from time *t* to time  $t + \Delta t$  by integrating the above

$$\chi au |_{t}^{t+\Delta t} - \int_{t}^{t+\Delta t} \chi d au = \int_{t}^{t+\Delta t} q d au$$

Approximating the integrals using the trapezoidal rule yields

$$\chi(z,\theta,t+\Delta t) = \chi(z,\theta,t) + (\frac{\Delta t}{2t+\Delta t})[q(z,\theta,t+\Delta t) + q(z,\theta,t)]$$

The resulting algebraic system is then solved iteratively.

## **Determination of Surface Vorticity**

The surface vorticity is determined by inverting the expressions for  $r_n$  and  $s_n$ . This leads to the truncated Fourier series

$$\zeta(0,\theta,t) = \frac{1}{M_0^2} \{ \frac{1}{2} s_0(0,t) + \sum_{n=1}^N [r_n(0,t)\sin(n\theta) + s_n(0,t)\cos(n\theta)] \}$$

The quantities  $s_n(0, t)$  and  $r_n(0, t)$  are computed by enforcing the integral conditions. That is, off the cylinder surface  $r_n$  and  $s_n$ can be computed using the most recent guess for  $\zeta$ . Then,  $s_n(0, t)$  and  $r_n(0, t)$  are computed by numerically satisfying the integral constraints.

# Summary of Numerical Algorithm

The following steps are performed ( $p \equiv$  iteration counter ): 1. solve for  $\phi^{(p)}(z, \theta, t + \Delta t)$ , 2. solve for  $\zeta^{(p)}(z, \theta, t + \Delta t)$  for  $z \neq 0$ , 3. compute  $r_n^{(p)}(z, t + \Delta t)$ ,  $s_n^{(p)}(z, t + \Delta t)$  for  $z \neq 0$ , 4. calculate  $r_n^{(p)}(0, t + \Delta t)$ ,  $s_n^{(p)}(0, t + \Delta t)$  by enforcing the integral conditions and hence compute  $\zeta^{(p)}(0, \theta, t + \Delta t)$ , 5. solve for  $f_n^{(p)}(z, t + \Delta t)$ ,  $F_n^{(p)}(z, t + \Delta t)$  and thus obtain  $\psi^{(p)}(z, \theta, t + \Delta t)$ ,

6. repeat above steps till convergence is reached and increment p by 1.

Convergence is reached when the difference between two successive iterates of the surface vorticity is less than  $\epsilon$ .

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**Computational Parameters** 

After performing numerous numerical experiments, the following computational parameters were chosen:

 $N = 25 \;,\; \epsilon = 10^{-6} \;,\; z_{\infty} = 10$ 

A typical grid size used was  $K \times L = 200 \times 120$ . Because of the impulsive start, small time steps of  $\Delta t = 10^{-3}$  were used initially. As time increased the time step was gradually increased to  $\Delta t = 0.05$ . Results were obtained using values

r = 0.5,  $\eta = 45^{\circ}$ , Pr = 0.7 for  $Gr = 10^{2}$  and  $Gr = 10^{4}$ 

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#### **Isotherm Plots**

Isotherm plot for  $Gr = 10^2, \eta = \frac{\pi}{4},$  Pr = 0.7, r = 0.5 at t = 2.5 (conduction regime).



#### **Isotherm Plots**

Isotherm plot for  $Gr = 10^2, \eta = \frac{\pi}{4},$  Pr = 0.7, r = 0.5 at t = 100 (well developed plume).



#### **Isotherm Plots**



#### **Isotherm Plots**



#### **Isotherm Plots**



#### Surface Vorticity Plots

Surface vorticity distributions for  $Gr = 10^4$ ,  $\eta = \frac{\pi}{4}$ , Pr = 0.7, r = 0.5.



#### Surface Temperature Plots

Surface temperature distributions for  $Gr = 10^4, \eta = \frac{\pi}{4}, Pr = 0.7, r = 0.5.$ 



# Analytical Validation

For large *Gr* and small *t* it is possible to expand the flow variables in the double series:

$$\chi = \chi_0 + \lambda \chi_1 + \lambda^2 \chi_2 + \cdots$$

where each  $\chi_n$  ( $n = 0, 1, 2, \cdots$ ) is further expanded:

 $\chi_n(z,\theta,t) = \chi_{n0}(z,\theta) + t\chi_{n1}(z,\theta) + \cdots$ 

The leading-order solution for the temperature is:

$$\phi(z,\theta,t) \sim \frac{2\sqrt{t}}{\sqrt{\pi Pr}\sqrt{Gr}} (e^{-PrM_0^2 z^2} - \sqrt{\pi Pr}M_0 z \operatorname{erfc}(\sqrt{Pr}M_0 z))$$

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#### Average Surface Temperature

Comparison of time variation of average surface temperature for  $Gr = 10^4, \eta = \frac{\pi}{4},$ Pr = 0.7, r = 0.5. Good agreement for small *t*; agreement worsens with time.



# **Concluding Remarks**

- Impulsively generated convection from an elliptic cylinder was investigated
- The numerical method presented is successful for computing unsteady flows for a wide range of Grashof numbers
- Numerical results were supported by analytical results
- The technique can be easily extended to handle other cross sections
- Future work includes comparisons with experiments ([4])

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